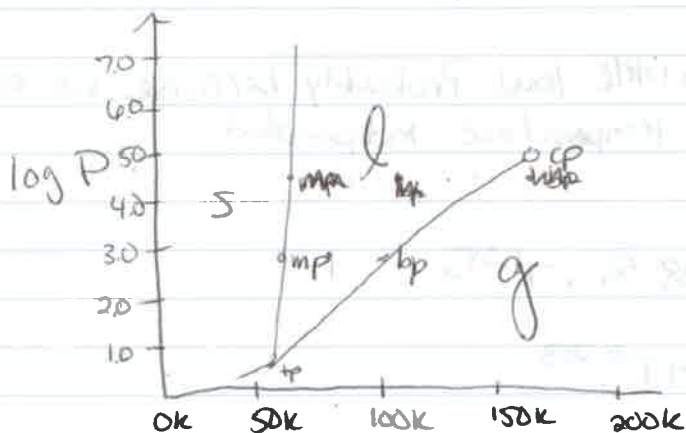


HWK #5 Key

1. Phase diagram for O_2

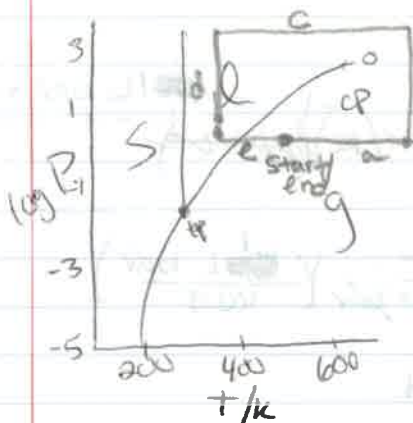
Triple pt: 54.3 K and 1.14 torr ($\log P = 0.569$)
 Critical pt: 154.6 K and 37828 torr ($\log P = 4.58$)
 Normal mp: 54.75 K and 760 torr ($\log P = 2.88$)
 normal bp: 90.25 K and 760 torr ($\log P = 2.88$)



side note
 No oxygen doesn't melt with applied pressure.
 - the solid-liquid coexistence curve has a positive slope (like benzene not H_2O).

2. Copy of Fig 23.5

1 atm $\Rightarrow \log(1) = 0$
 500 atm $\Rightarrow \log(500) = 2.699$



- (a) start as gas, end as hotter gas
- (b) move into supercritical phase
- (c) cool from supercritical phase to liquid phase
- (d) stay in liquid phase but @ reduced pressure
- (e) end at beginning pt (gas)... vaporization observed

3. Clausius-Clapeyron Equation

$$\ln P_2/P_1 = \frac{-\Delta_{\text{vap}}H}{R} \left(\frac{1}{T_2} - \frac{1}{T_1} \right)$$

normal = 1 atm

n top of H₂O = 100°C = 373 K

110°C = 383 K

$$\ln P_2/1 \text{ atm} = \frac{-40650 \text{ J/mol}}{8.314 \frac{\text{J}}{\text{mol}\cdot\text{K}}} \left(\frac{1}{383 \text{ K}} - \frac{1}{373 \text{ K}} \right)$$

$$P_2 = e^{0.342} = 1.41 \text{ atm or } 1070 \text{ torr}$$

Our value is a little low. Probably because we assumed $\Delta_{\text{vap}}H$ was temperature independent.

4. $P = -718 + 2.38565 T^{1.283}$

$$\frac{dP}{dT} = 3.06079 T^{0.283}$$

$$\frac{dP}{dT} @ 85.46 \text{ K} = 10.778 \text{ bar/K}$$

$$\frac{dP}{dT} = \frac{\Delta \bar{H}}{T \Delta \bar{V}}$$

$$\Delta \bar{V} = \frac{\Delta \bar{H}}{T} \cdot \left(\frac{dP}{dT} \right)^{-1}$$

$$= \frac{35300 \text{ J/mol}}{85.46 \text{ K}} (10.778 \text{ bar/K})^{-1}$$

1 L · bar = 100 J

$$= \frac{35300 \text{ J/mol}}{85.46 \text{ K}} \left(38.32 \frac{\text{J}}{\text{mol}\cdot\text{bar}} \right) \left(\frac{1 \text{ L}\cdot\text{bar}}{100 \text{ J}} \right)$$

$$= 0.3832 \text{ L/mol}$$

5. See attached Excel sheet

$$\Delta_{\text{vap}}H = \Delta H_g - \Delta H_l = 47.8100 - 0.5509 = 35.2591 \text{ kJ/mol}$$